

# Advanced wastewater treatment system for high BOD wastewater

Enzyme activated method

CM System • CMS System

Catalysis + Microorganism + Support

CMS System: Japan Patent No. 595023

## Technology description

### Overseas Sales Dep

Sales agency : Tomoe Engineering Co., Ltd.  
Osaki Bright Core, 5-15 Kitashinagawa 5-chome,  
Shinagawa-ku, Tokyo 141-0001, Japan  
Tel : +81 3 3442 5157 Fax : +81 3 3442 5179

URL <http://www.tomo-e.co.jp>

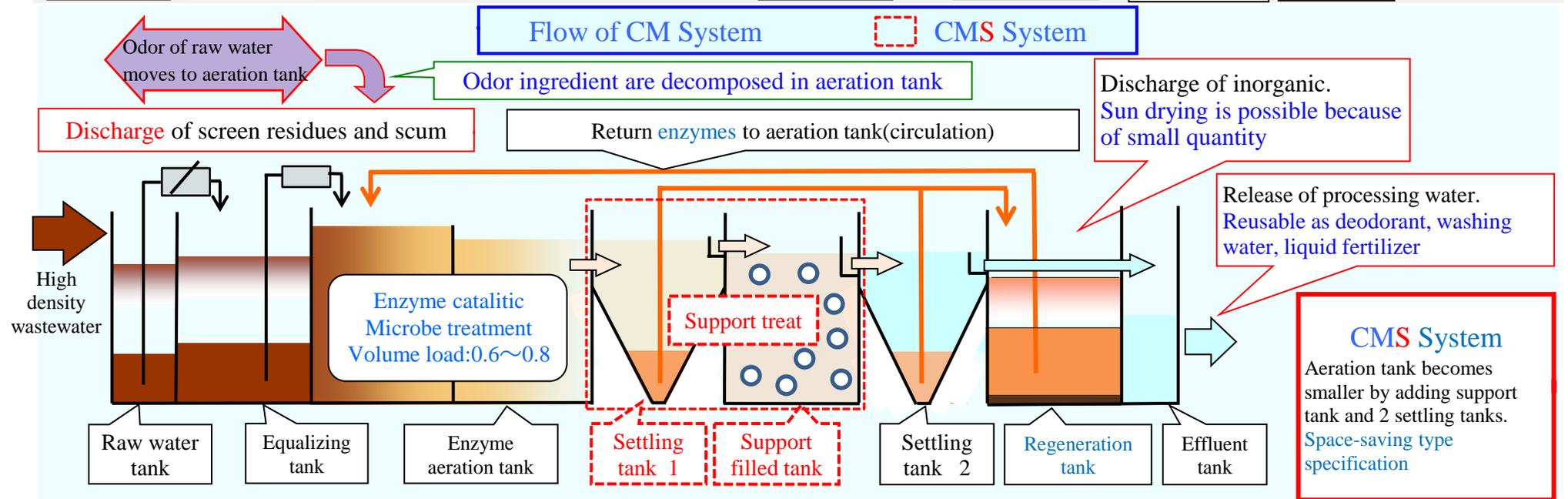
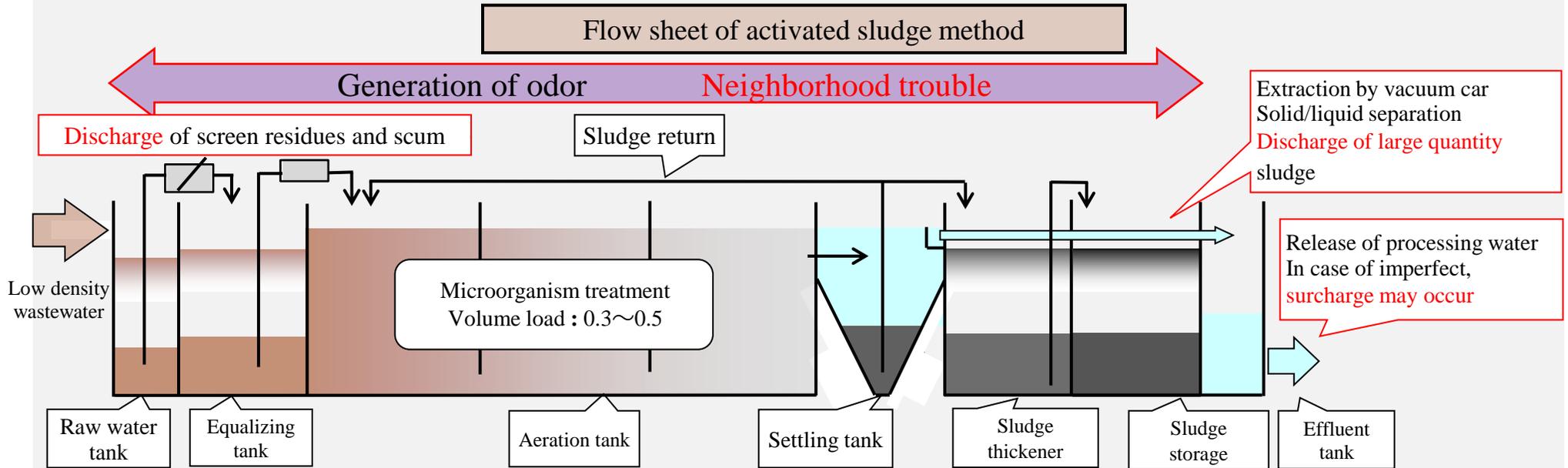
E-mail [overseas@tomo-e.co.jp](mailto:overseas@tomo-e.co.jp)

Manufacturer : Jfils Ltd.  
5-12-30, Nakai Kokurakita-ku Kitakyushu-city,  
Fukuoka Prefecture 803-0836, Japan

URL <http://www.jfils.jp>

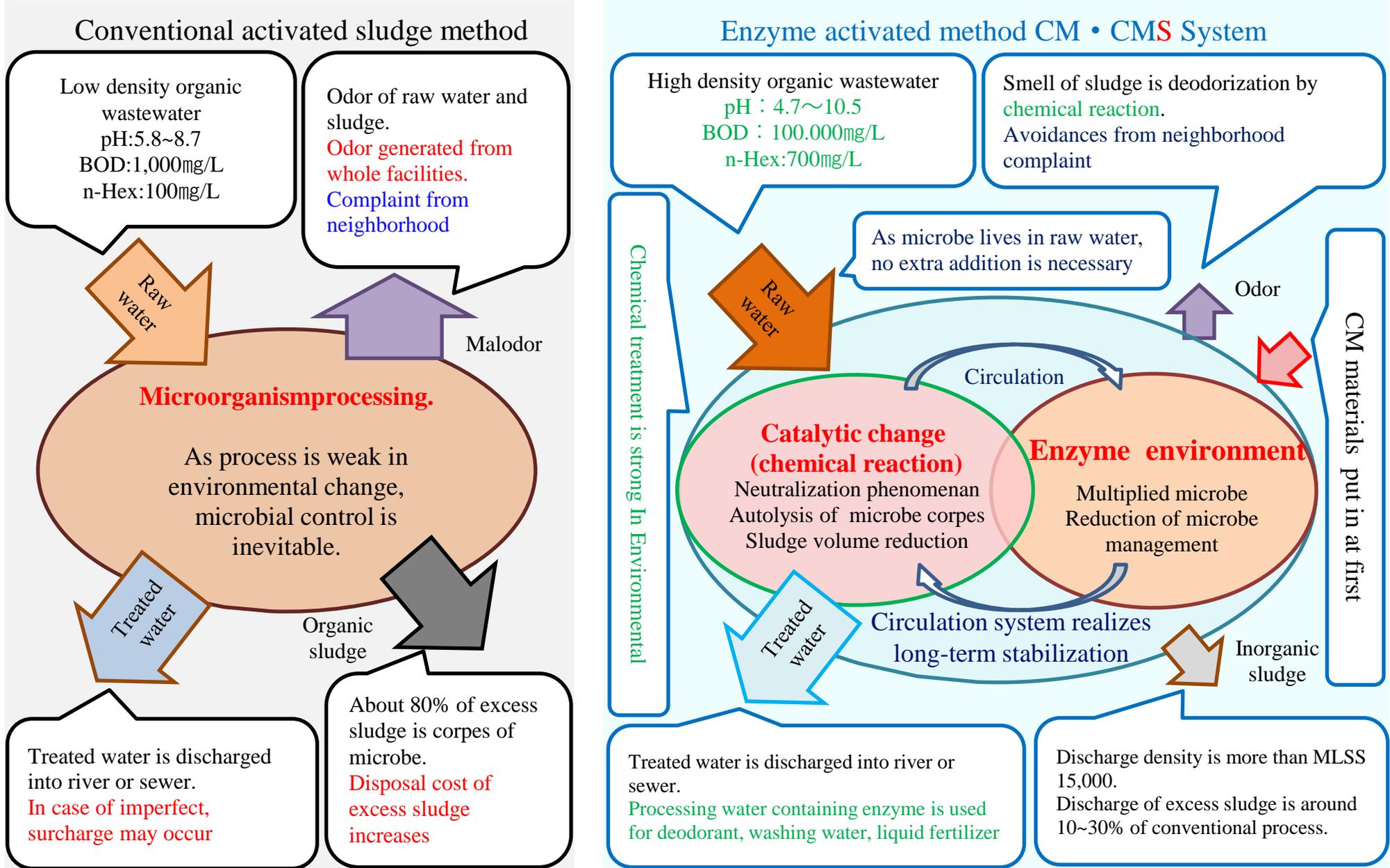
# Difference between conventional activated sludge method and enzyme activated method

## 1. Hardware side

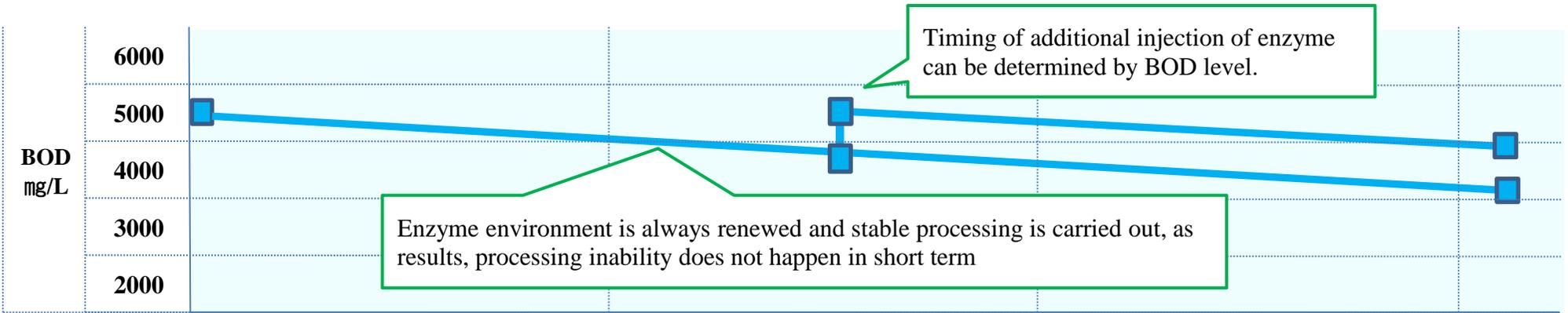
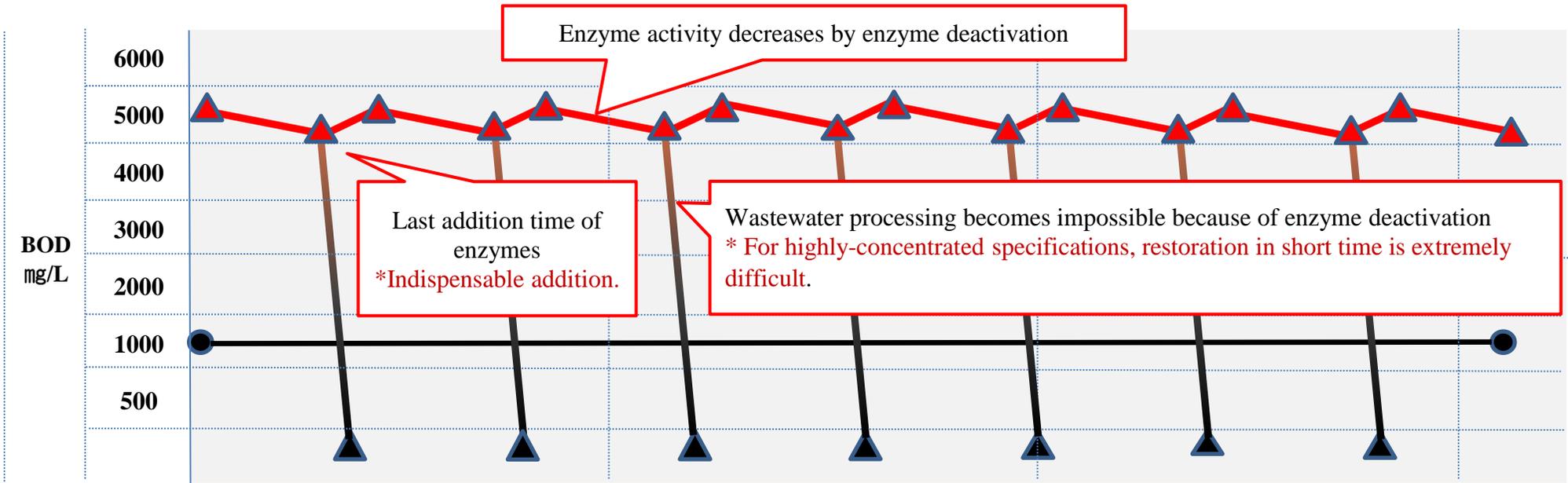


# Difference between conventional activated sludge method and enzyme activated method

## 2. Software side



## Difference between consecutive enzyme addition method and CM System.



## Difference between latest activated sludge method and enzyme activated method

### 3. Initial and running cost

Raw water: Organic wastewater		Latest activated sludge method	CM • CMS System		
Processing capacity	BOD mg/L	Max.4,000~7,000	100,000 (there is no upper limit theoretically)		
	pH	5.8~8.7	4.7~10.5 (in case short time 4~11)		
	n-Hex mg/L	100	Even 700 becomes less than 1 (actual performance)		
Disposal expense of excess sludge		assume 100%	Less than 10~30%		
Initial	Middle density	No-pretreatment BOD : 7,000 pH : 7 n-Hex:100	assume 100%	110~120%	Reference level
Running		assume 100%	Amlount of excess sluge : 10~30% Total : 70~80%	Reference level	
Initial	High density	No-pretreatment BOD : 9,000 pH : 4.7 n-Hex:500	Unfeasible	90~100% of activated method	Reference level
Running		Amount of excess sludge : 10~30% Total : 30~50%		Reference level	

### Practical example : Comparison of annual running cost. Object: Food-processing factory drainage

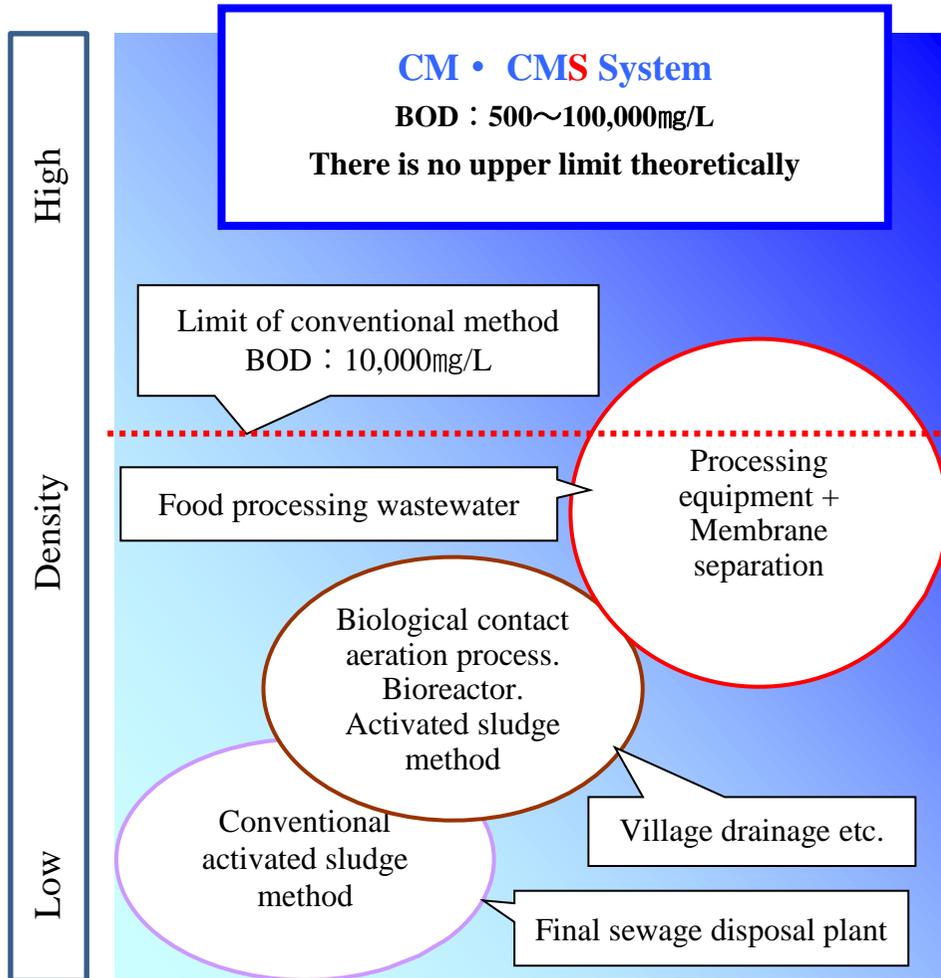
Unit: thousand yen

Specification : Flow rate:50ton/day, BOD=4,500, COD=3,000, n-Hex-700, pH=4.7

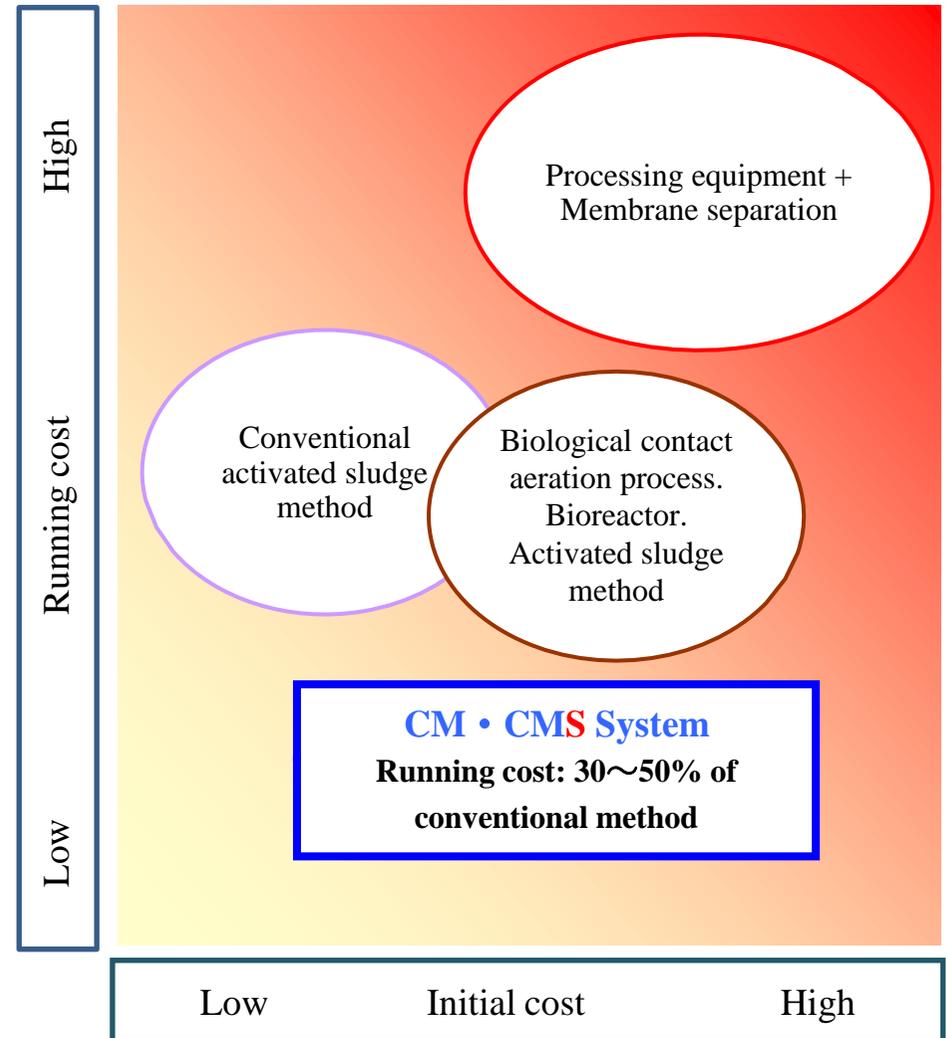
	Chemical expense	+	Sludge disposal cost	+	Necessary cost	+	Administration cost	=	Total	Machine update cost (future)	
Acivated method	1,800	+	3,750	+	500	+	1,000	=	7,050	15,000 (Dehydrater etc)	
<b>CMS System</b>	0	+	1,200	+	0	+	1,700	=	2,900	0	
Residue, scum and excess sludge							Amount of annual reduction = 4,150 thousand Yen				

# Positioning

## Capacity



## Cost



## Marketing

### Industries having problems

Confectionery production

Cooling drinks

Meat processing

Dairy products production

Fishery products processing

Starches processing (Soy sauce, Tofu )

Others. Hog raising business. Shochu brewing

### Problem content

1、 Because density is high, handle as industrial waste disposal

**Problem** : Expensive industrial waste processing cost. Anxious whether appropriate disposal is done or not

2、 Whether existing processing equipment attain effluent standard or not

**Problem** : Cost rise due to surcharge. Uneasiness for surprise inspection

3、 Chemical expense. Machine purchase costs

**Problem** : Excess sludge disposal costs. Flocculant costs. Renewal cost such as apparatuses

4、 Malodor

**Problem** : Anxious about odor pollution to neighborhood

**Recently, issue of malodor becomes remarkable**

## Facilities summary

New construction : Treatment of factory effluent

**CM System** : Smaller than conventional sludge method (10-15% decrease) \* Stable operation in volume load 0.6-0.8

**CMS System** : More smaller in case of support treatment (20~30% decrease) \* Support becomes bio organism bed

Concrete • aboveground, semi-basement, underground Steel and Stainless steel • aboveground

New construction : Reprocessing of excess sludge

Effective for volume-reduction of large amount of excess sludge

**CM • CMS** : Disposal of microbe's corpse existing in excess sludge before dehydration \*Volume reduction rate : 50~80%



Reinforced concrete aboveground facility



Reinforced concrete semi-basement facility



Existing diversion. Steel structure



Existing diversion : Perfect zymogenesis

Remodel of existing facilities into complete zymogenesis is possible, in case shutdown is possible during necessary period.

Existing diversion : Zymogenesis by enlargement of regeneration tank

Zymogenesis is possible by addition of regeneration tank, in case short time shutdown is possible.

Existing diversion : Semi-zymogenesis changing to by-pass process

Change to semi-zymogenesis is possible by addition of small CM system, in case shutdown is not permitted.

Principle of by-pass method : 10% of raw water is treated by enzyme processes of bypass, therefore load of facilities is reduced by 10%.

Processing water goes back up to existing aeration tank.

Consecutive insertion of water containing enzymes stabilizes operation and reduce excess sludge.

## Sales framework, Maintenance & Administration structure

### Sales framework

Base of domestic sale :Fukuoka-Pref., Saga-Pref. and Tokyo      Base of overseas sale : Fukuoka-Pref. and Tokyo

Sale area:Japan and foreign countries

Sales results until 2016:Tochigi ~ Okonawa, Pref. 21 facilities. Proof experiment: 3 (in Oversea), 4 (in Japan)

Sales plan in 2017: 2 facilities (in Japan), 1 facility (in Vietnam), more than 5 test plants (Domestic and abroad)

Future sale plan to abroad: Vietnam, India, Indonesia and others. Developed countries

### Maintenance system

When problem is not settled locally, we dispatch our employees from head office and deal with.

When maintenance takes time, we ask for cooperation of client or subcontractor

When local correspondence is possible, we ask for handling of client or subcontractor themselves

Please give us notice over telephone

In case of oversea : Our local subcontractor will cope. We are ready to deal through telephone and E-mail

### Administration system

Client, subcontractors of client, our subcontractors, local management companies handle.

After trial run, we carry out management training to concerned parties

## Past results

Introduction body	Area	Kind of drainage	Flow rate (m <sup>3</sup> /D)	BOD(mg/L)	Influent pH	Discharge	
G Food	Kansai	Food processing	150	1,300	5.2	River	New construction
O Stock raising	Kyushu	Hog raising	25	8,500	6.2	River	Existing diversion
H Food	Kansai	Food processing	400	1,600	5	River	New construction
U Stock raising	Kyushu	Hog raising	12.5	9,000	8.9	River	New construction
S Food	Chubu	Food processing	30	1,100	6	River	Existing diversion
S Food	Chubu	Food processing	60	1,300	5.2	River	Existing diversion
H Processing	Kantou	Lavation	900	1,800	11~4.5	River	Existing diversion
F Association	Kyushu	Starch production	240	1,300	5.2	River	New construction
S Food	Kyushu	Food processing	60	4,500	3.5~5.3	Sewage	New steel made
K Recycling	Kyushu	Food processing	1.2	3,000	4.0	Sewage	Existing diversion
K Food	Kyushu	Food processing	20	800	4.0	River	Existing diversion
C Drink	Kyushu	Drinking water	5	1,000	4.0	On-site	New construction

Several others



Sampling at residues screen  
Cloudy



Sampling at No.1 aeration tank  
Deposition : Enzyme materials and floc



Sampling at support filled tank (S System)  
Floating matter: support



Sampling at final settler  
Approx. transparent

# Verification survey by demonstration experiment Example: High density wastewater from sweet potato shochu brewing factory

Test-plant of Jfils



Experimental equipment : CM120L

Test-plant of client



Shochu brewing in Miyazaki Pref.  
Experiment period: 35 days

※2

※3

許業証明書

許業番号: 4-00000  
発行: 2017年06月27日

公認計測士 高橋洋太郎  
公認計測士事務所 高橋洋太郎事務所  
〒880-0001 宮崎県宮崎市南宮崎1-1-1

測定項目: BOD

項目	単位	測定値	許容範囲	測定日時
生体酸素消費量 (BOD)	mg/L	63,000	100,000	2017.06.27
化学的酸素消費量 (COD)	mg/L	100,000	100,000	2017.06.27
総窒素 (TN)	mg/L	100	100	2017.06.27
総リン (TP)	mg/L	10	10	2017.06.27
濁度 (Turbidity)	mg/L	100	100	2017.06.27
pH		4.0	4.0	2017.06.27

Before processing

許業証明書

許業番号: 4-00000  
発行: 2017年06月27日

公認計測士 高橋洋太郎  
公認計測士事務所 高橋洋太郎事務所  
〒880-0001 宮崎県宮崎市南宮崎1-1-1

測定項目: BOD

項目	単位	測定値	許容範囲	測定日時
生体酸素消費量 (BOD)	mg/L	7.3	100,000	2017.07.10
化学的酸素消費量 (COD)	mg/L	100	100,000	2017.07.10
総窒素 (TN)	mg/L	100	100	2017.07.10
総リン (TP)	mg/L	10	10	2017.07.10
濁度 (Turbidity)	mg/L	100	100	2017.07.10
pH		7.6	7.6	2017.07.10

After processing

Analytical values by client

※1

濃度計量証明書

計測番号: 4-00000  
発行: 2017年06月27日

公認計測士 高橋洋太郎  
公認計測士事務所 高橋洋太郎事務所  
〒880-0001 宮崎県宮崎市南宮崎1-1-1

測定項目: BOD

項目	単位	測定値	許容範囲	測定日時
生体酸素消費量 (BOD)	mg/L	38,000	100,000	2017.06.27
化学的酸素消費量 (COD)	mg/L	100,000	100,000	2017.06.27
総窒素 (TN)	mg/L	100	100	2017.06.27
総リン (TP)	mg/L	10	10	2017.06.27
濁度 (Turbidity)	mg/L	100	100	2017.06.27
pH		4.1	4.1	2017.06.27

Raw water BOD : 38,000mg/L pH:4.1

Analytical values by Jfils



Three hours progress

Objective	High-concentrated waste fluid processing • No-discharge process
Experimental equipment	CM120L (BOD : 1,000mg/L • hour = 120L/day)
Analysis by Jfils	Raw water BOD : 38,000mg/L pH:4.1 ※1
Before processing	Raw water BOD : 63,000mg/L pH:4.0 ※2
After processing	Treated water BOD : 7.3mg/L pH:7.6 ※3
Throughput	Raw water (3L/Day) is diluted with processing water (30L/Day) No discharge experiments
Test period	35 days experiment by client Jfils carried out only setting and removal of facilities
Comment of president	Wonderful result was beyond my expectation. I'd like to enhance this technology to many companies having problems on high density wastewater treatment